

Driving the **global energy transition** with green hydrogen

Electrolyzers for "dummies"



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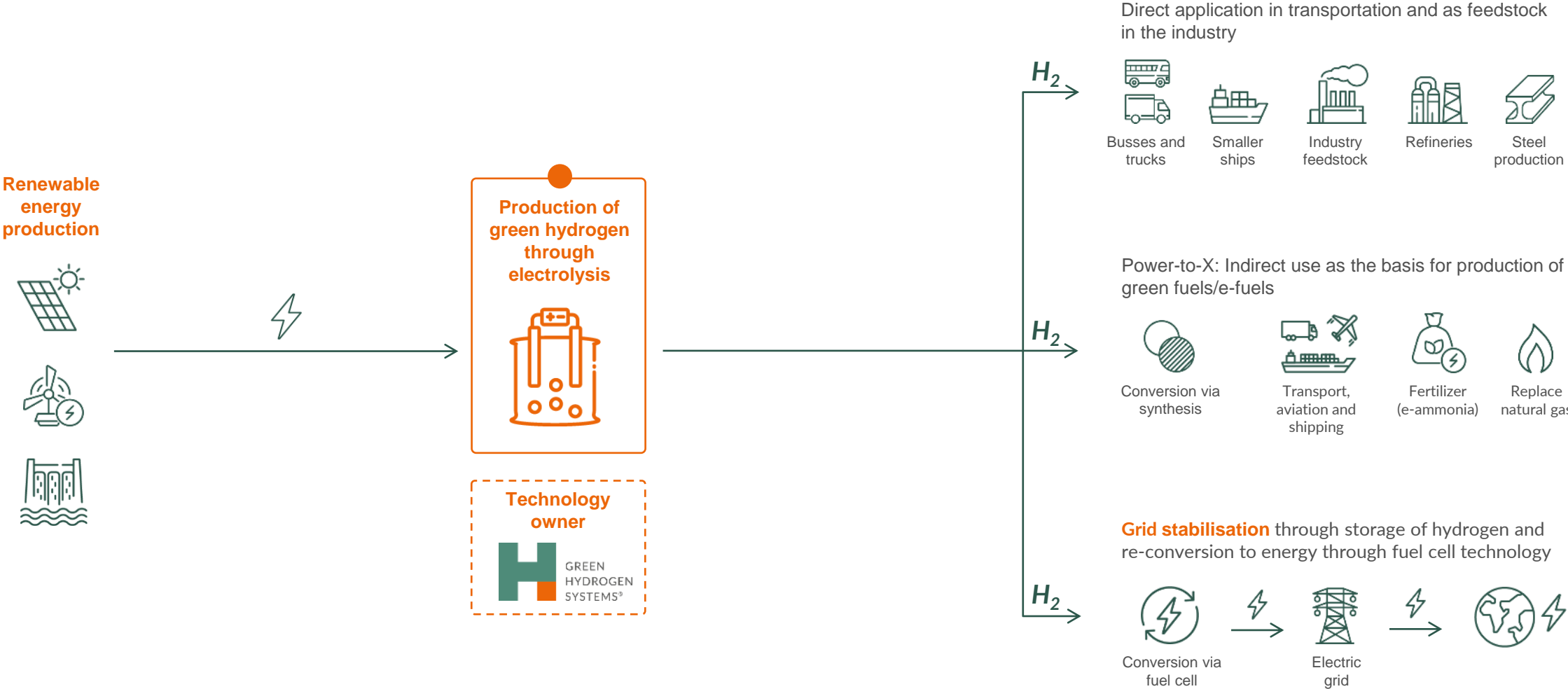
General

Introduction

The why

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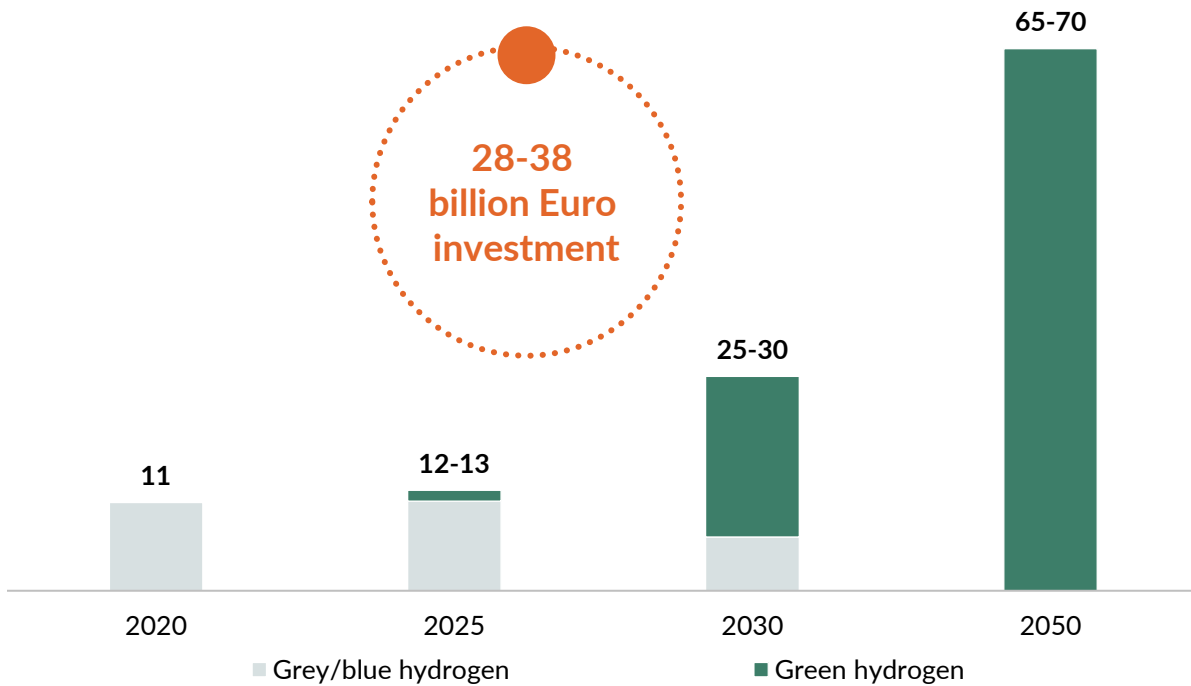
Green hydrogen's role in the future energy system



Increased electrolyser demand

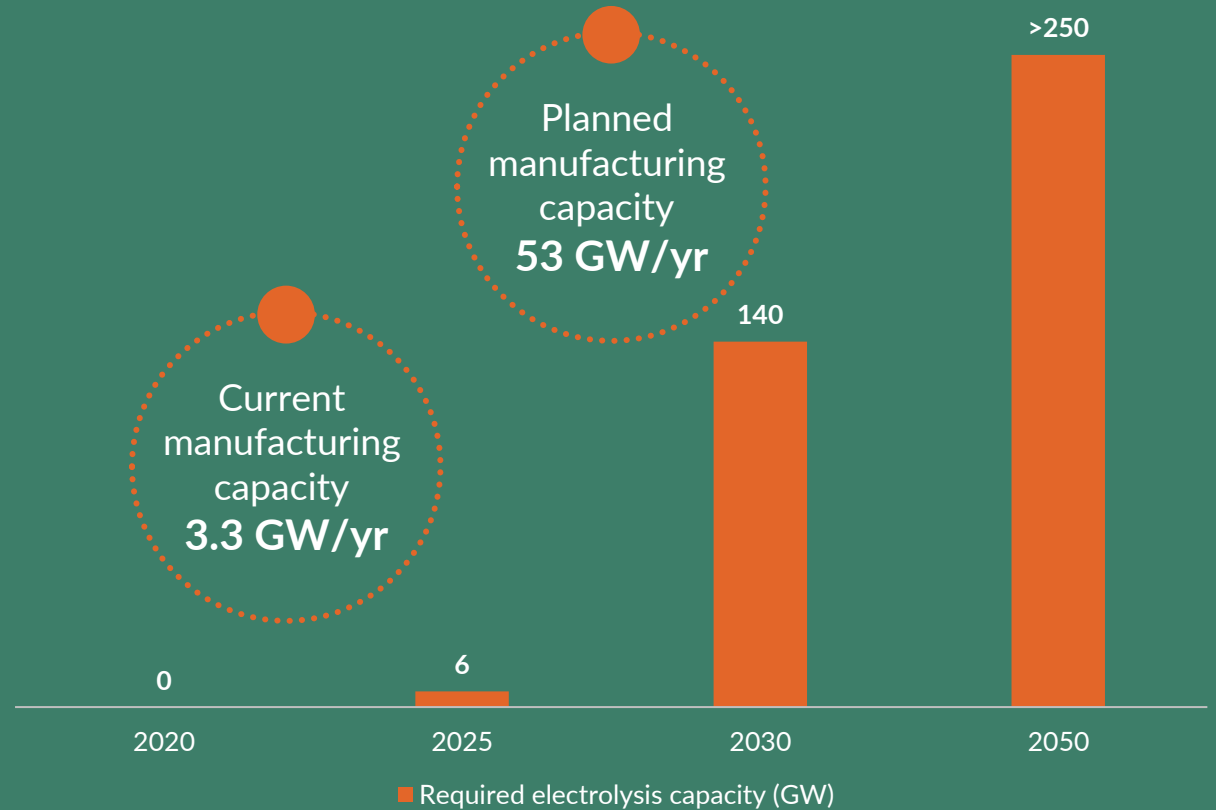
Estimated future demand for hydrogen in the EU

From Dansk Energi. Hydrogen demand in million tonnes H2 2021; Clean Hydrogen Monitor 2022, Hydrogen Europe; REPowerEU, EU 2022



Demand for hydrogen in Europe is expected to grow significantly

Required electrolysis capacity to meet EU demand



To meet demand, manufacturing capacity must increase considerably

Levelized Cost of Hydrogen

- Cost contributors example*

- CAPEX 15-25%
- Efficiency 60-80%
- OPEX 5-15%

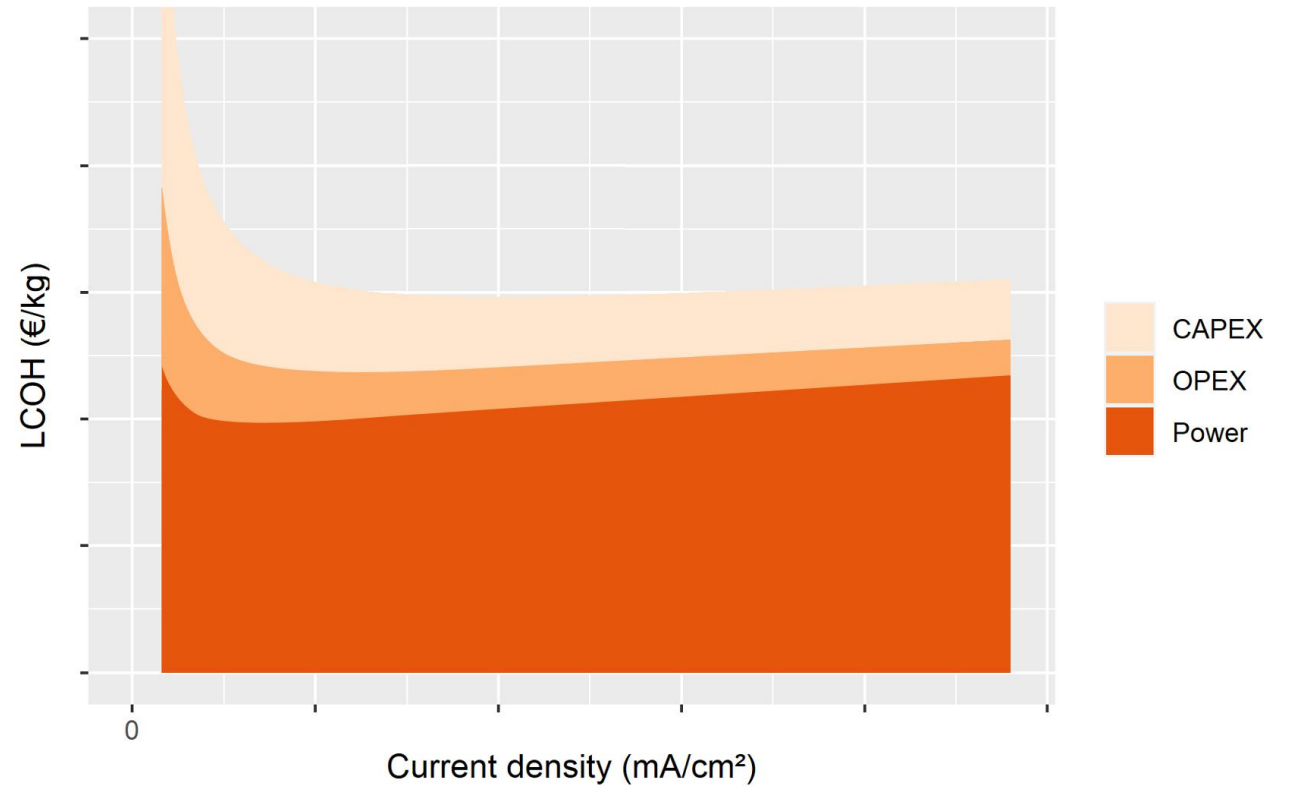
$$\text{LCOH} = \frac{\text{Costs}}{\text{H}_2 \text{ production}}$$

* Electricity spot prices from Denmark's electricity grid in 2023, 75% utilization

Levelized Cost of Hydrogen

- Cost contributors example*
 - CAPEX 15-25%
 - Efficiency 60-80%
 - OPEX 5-15%
- LCOH insights give strategy to lower LCOH
- LCOH insights can be counter-intuitive
- Note: added value from increased pressure not included in LCOH

$$\text{LCOH} = \frac{\text{Costs}}{\text{H}_2 \text{ production}}$$



* Electricity spot prices from Denmark's electricity grid in 2023, 75% utilization

Levelized Cost of Hydrogen

- Improving the picture: using several value streams
- Hydrogen
- Oxygen
- Waste heat

$$\text{LCOH} = \frac{\text{Costs}}{\text{H}_2 \text{ production}}$$



$$\text{LCOH} = \frac{\text{Costs}}{\text{H}_2 \text{ production} + \text{O}_2 \text{ production} + \text{waste heat}}$$

HyProvide[®] A-Series ■

A modular, containerized, plug-and-play electrolysis solution

Current offering

- Two product variants: A180 (900kW)
- Hydrogen production: 180 Nm³/hr – (16 kg)
- Hydrogen gas purity: 99.998 %
- Cell stack: 53 kWh/kg
- Cell stack + Stack Power Supply (SPS): 57 kWh/kg H₂
- Hydrogen outlet pressure: 30 barg.

0.9 MW



A180, two stacks of 450kW each, in a 40 foot container
(includes auxiliary systems)

HyProvide[®] X-Series ■

A modular, scalable electrolysis solution in enclosure

Under commissioning

- One product variant: X1200 (6 MW)
- Hydrogen production: 1,200 Nm³/hr (107 kg)
- Hydrogen gas purity: 99.998 % (with GTO)
- Cell stack: 53 kWh/kg H₂
- Cell stack + Stack Power Supply (SPS): 57 kWh/kg H₂
- Hydrogen outlet pressure: 35 barg.

6 MW



Enclosure comprising 1x X1200 unit
(auxiliary systems incl. Deoxo, Dryer and Dry cooler are optional)

Electrolysis

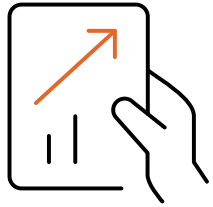
The how



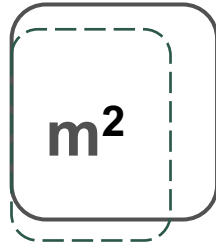
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How to choose between electrolyser technologies

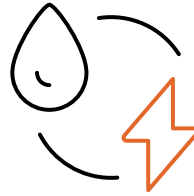
Specific customer requirements will lead to different choices



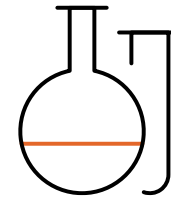
Project size (MW)



Footprint



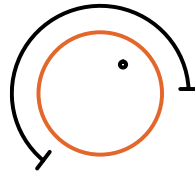
Material use



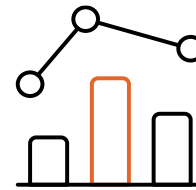
Hydrogen quality



TCO / business case

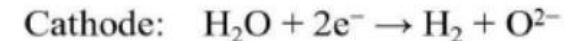
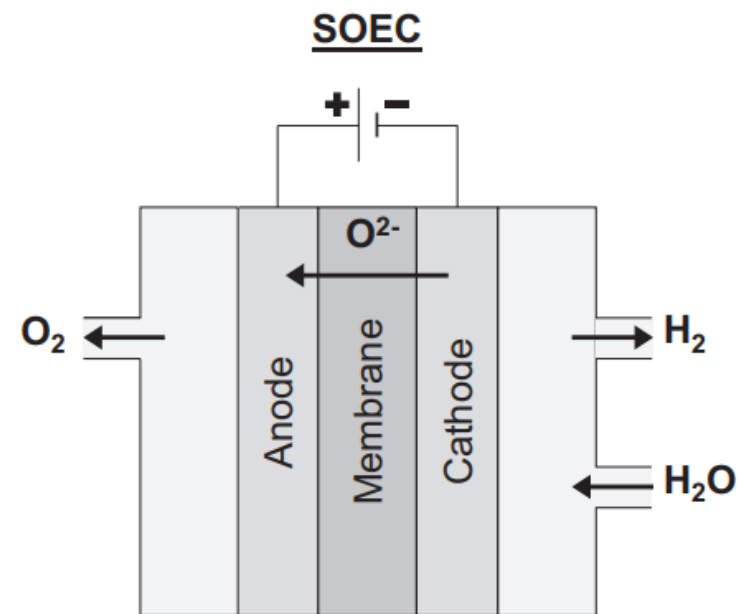
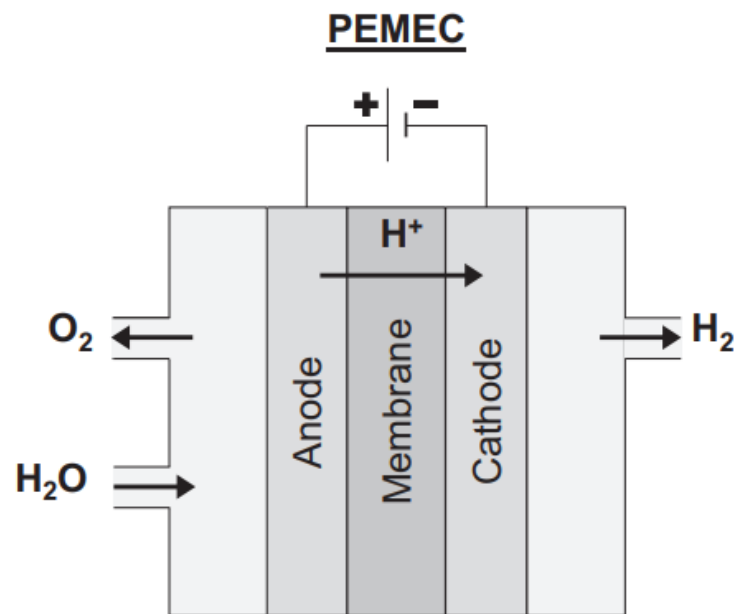
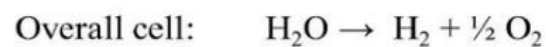
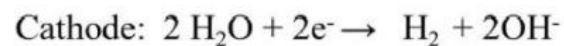
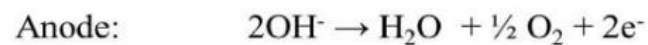
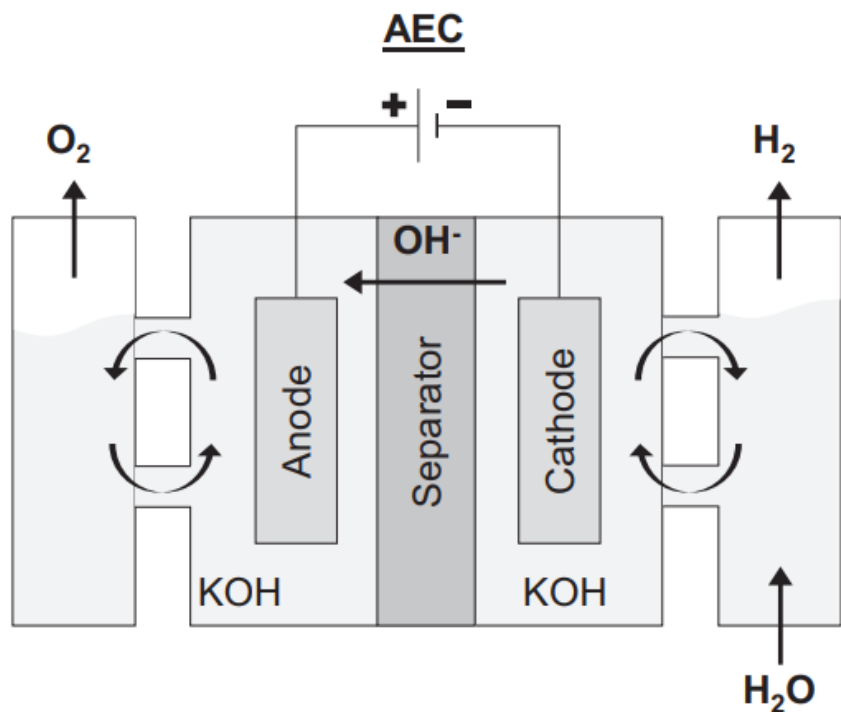


Hydrogen pressure



Dynamic response

Technologies



Detailed Technology Comparison

Table 1 – Main characteristics of AEC, PEMEC and SOEC systems.

	AEC	PEMEC	SOEC
Electrolyte	Aq. potassium hydroxide (20–40 wt% KOH) [9,32,33]	Polymer membrane (e.g. Nafion) [33,34]	Yttria stabilised Zirconia (YSZ) [37,38]
Cathode	Ni, Ni-Mo alloys [9,32,33]	Pt, Pt-Pd [34]	Ni/YSZ [37,38]
Anode	Ni, Ni-Co alloys [9,32,33]	RuO ₂ , IrO ₂ [34]	LSM ^b /YSZ [37,38]
Current density (A cm ⁻²)	0.2–0.4 [34]	0.6–2.0 [34]	0.3–2.0 [9,38]
Cell voltage (V)	1.8–2.4 [34]	1.8–2.2 [34]	0.7–1.5 [38]
Voltage efficiency (% _{HHV})	62–82 [34]	67–82 [34]	<110 [33]
Cell area (m ²)	<4 [33]	<0.3 [33]	<0.01 [33]
Operating Temp. (°C)	60–80 [34]	50–80 [34]	650–1000 [37,38]
Operating Pressure (bar)	<30 [33]	<200 [33]	<25 [33]
Production Rate ^c (m ³ _{H₂} h ⁻¹)	<760 [33]	<40 [33]	<40 [33]
Stack energy ^c (kWh _{el} m ³ _{H₂} ⁻¹)	4.2–5.9 [34]	4.2–5.5 [34]	>3.2 [33]
System energy ^c (kWh _{el} m ³ _{H₂} ⁻¹)	4.5–6.6 [16]	4.2–6.6 [16]	>3.7 (>4.7) _{kWh_{energy}} ^a
Gas purity (%)	>99.5 [32]	99.99 [33]	99.9 ^a
Lower dynamic range ^d (%)	10 – 40 [33,34]	0 – 10 [34]	>30 ^a
System Response	Seconds [33]	Milliseconds [33]	Seconds ^a
Cold-start time (min.)	<60 [16]	<20 [16]	<60 ^a
Stack Lifetime (h)	60,000–90,000 [16]	20,000–60,000 [16]	<10,000 ^a
Maturity	Mature	Commercial	Demonstration ^a
Capital Cost (€ kW _{el} ⁻¹)	1000–1200 [16]	1860–2320 [16]	>2000 [16]

^a Where no reference is provided, data were derived during expert elicitations.

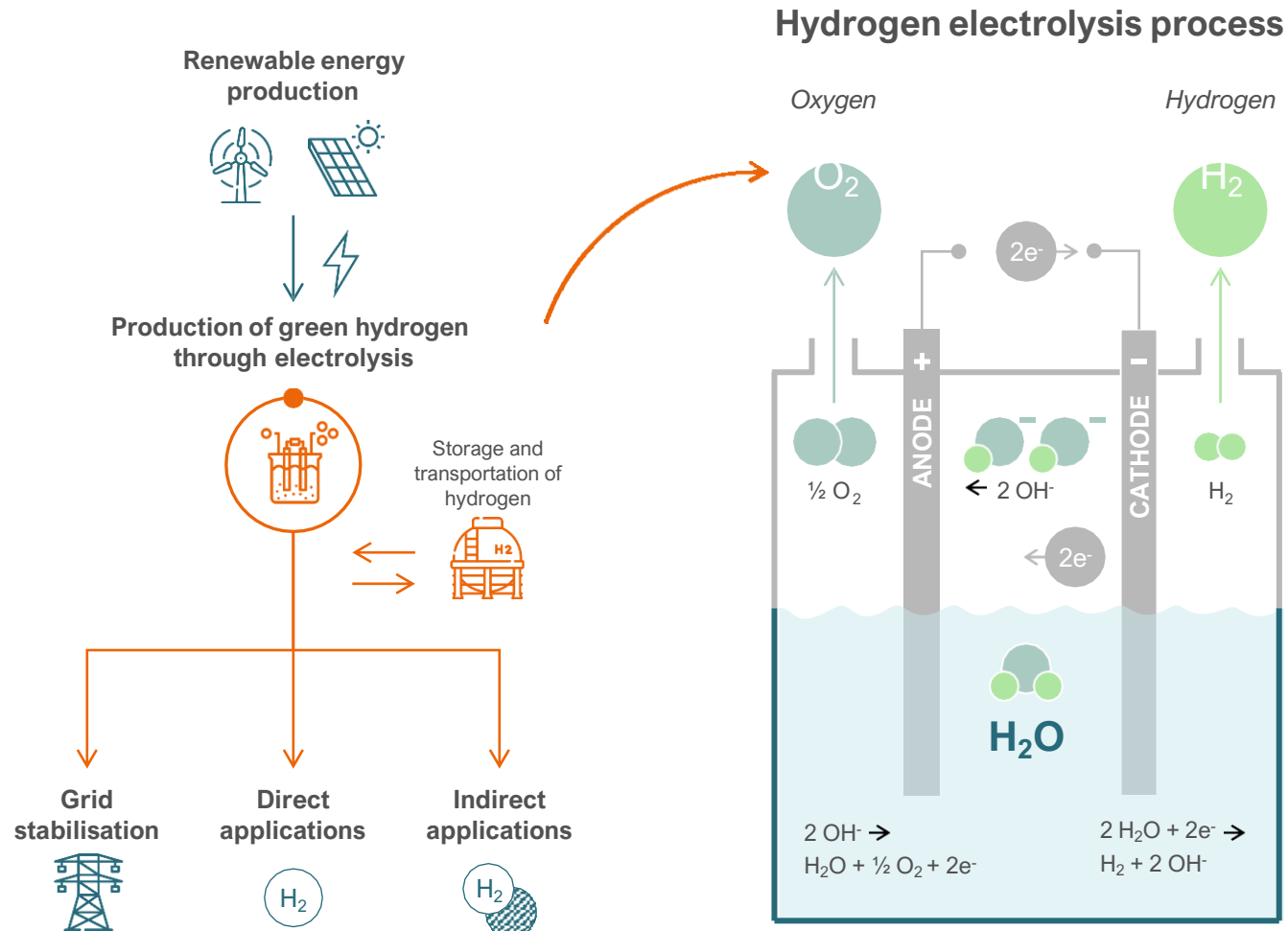
^b Perovskite-type lanthanum strontium manganese (La_{0.8}Sr_{0.2}MnO₃).

^c Refers to norm cubic meter of hydrogen (at standard conditions) and respective electrical energy consumption (kWh_{el}) if applicable.

^d Minimum operable hydrogen production rate relative to maximum specified production rate.

Pressurized Alkaline Electrolysis

Splits water into hydrogen and oxygen



Hydrogen electrolysis is a process that splits water into hydrogen and oxygen using electricity.

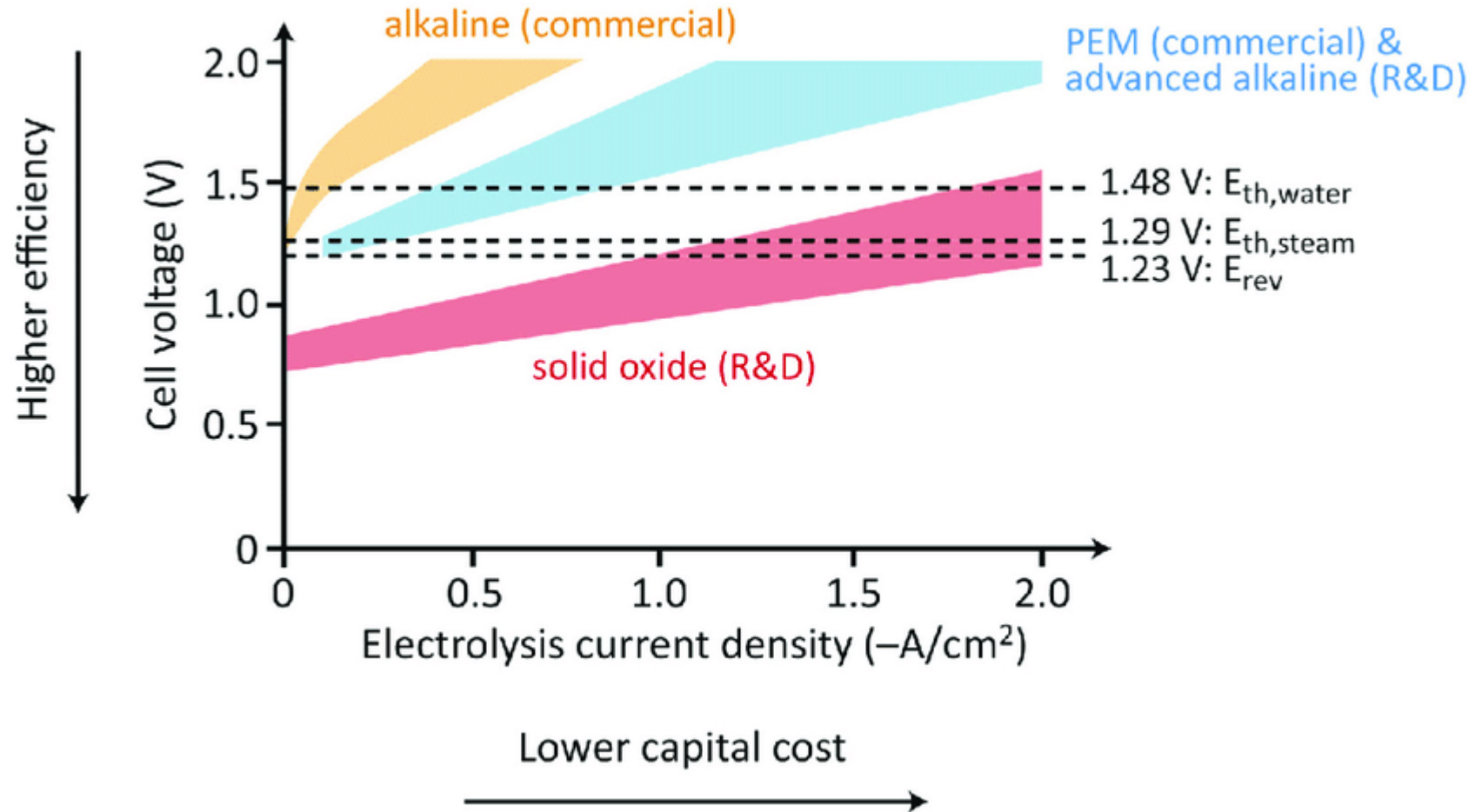
Hydrogen generated from renewable electricity sources is considered **green hydrogen**.

The process of green hydrogen electrolysis is completely fossil-free, as the only by-product is oxygen and the power used in electrolysis is generated from renewable sources.

Pressurized

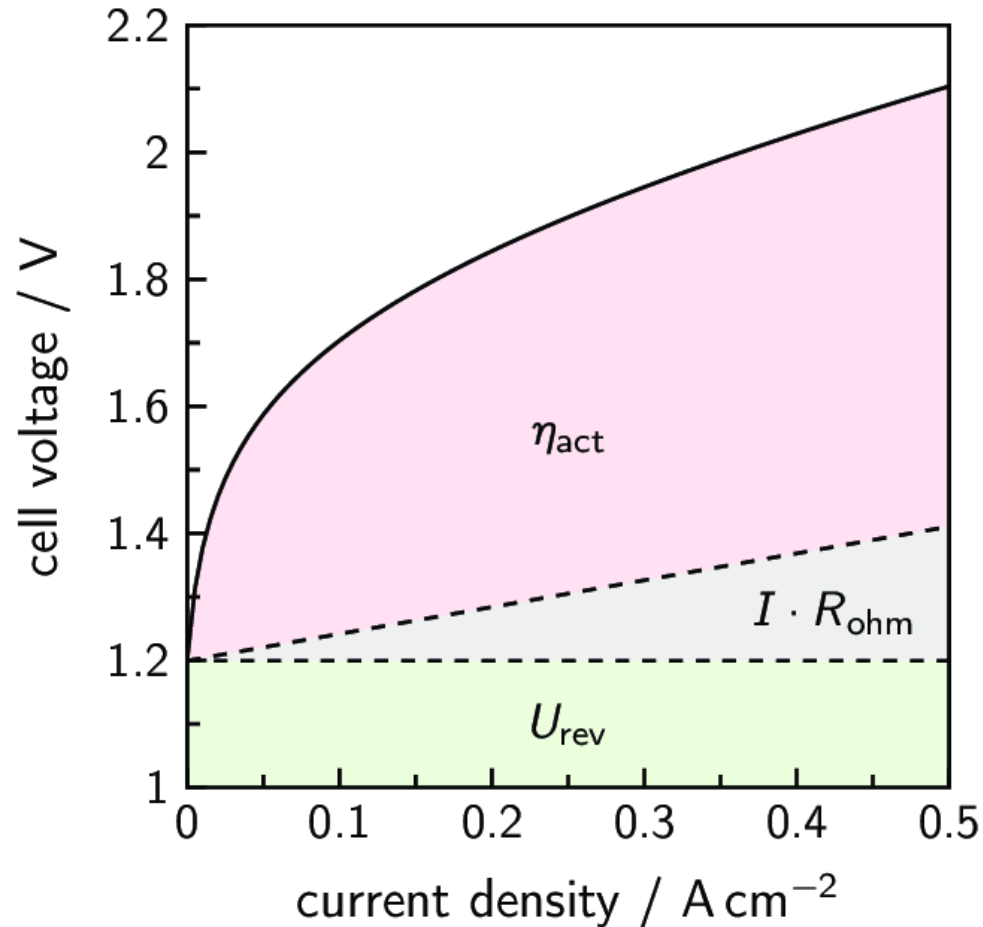
Electrolysis

Splits water into hydrogen and oxygen



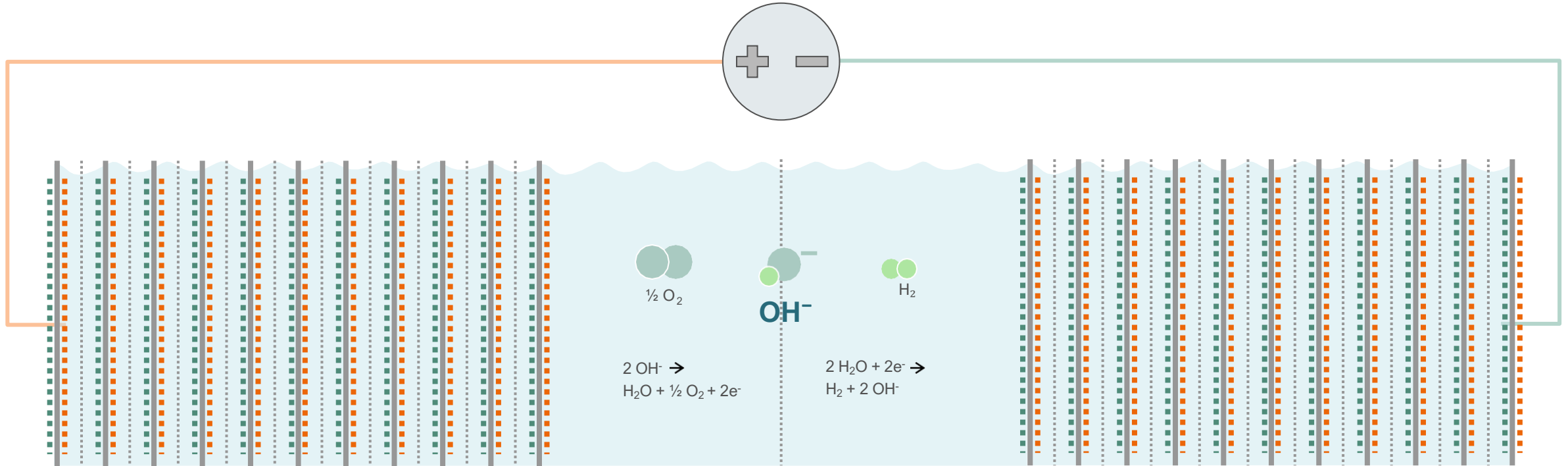
Pressurized Alkaline Electrolysis

Splits water into hydrogen and oxygen



- Activation losses (improvement possible from higher T and catalyst on anode/cathode)
- Resistive losses (diaphragm, circuit, bubbles, electrolyte etc)
- Reversible cell voltage (1.23 V, electrolysis of vapour H₂O)
- Not shown: starting from liquid water (U_{rev} from 1.48 V)

Pressurised (Alkaline) Electrolysis



Zero-gap design – combines numerous electrochemical cells into a stack of cells.

All cells are wetted with electrolyte (pH > 14), which is in turn saturated with hydrogen and oxygen. Electrolyte circulated through system.

Resulting in

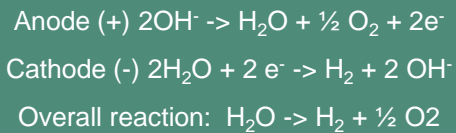
- High area with small design
- Few electrical connections
- Higher voltage with the same current

Challenges

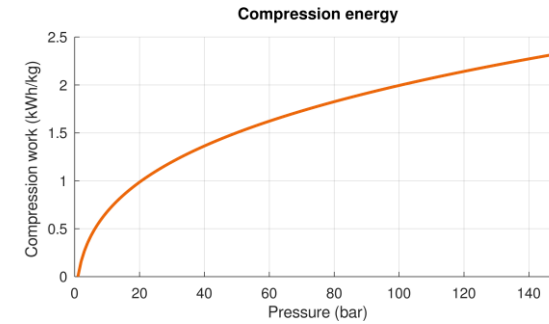
- Highly corrosive environment
- Conducting electrolyte will draw stray currents

Pressurized (Alkaline) Electrolysis

Electrolyser as pressure vessel
Using the electrochemical reactions to pressurize the system

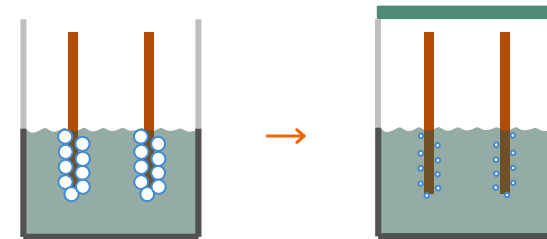


System efficiency
The overall energy demand for producing pressurized hydrogen can be reduced by utilizing the nature of the electrolyser.



Reduced gas volume

- Dynamic behaviour: Fast ramp rates enable coupling to RE sources.
- Footprint: Greatly reduced by increasing gas density.



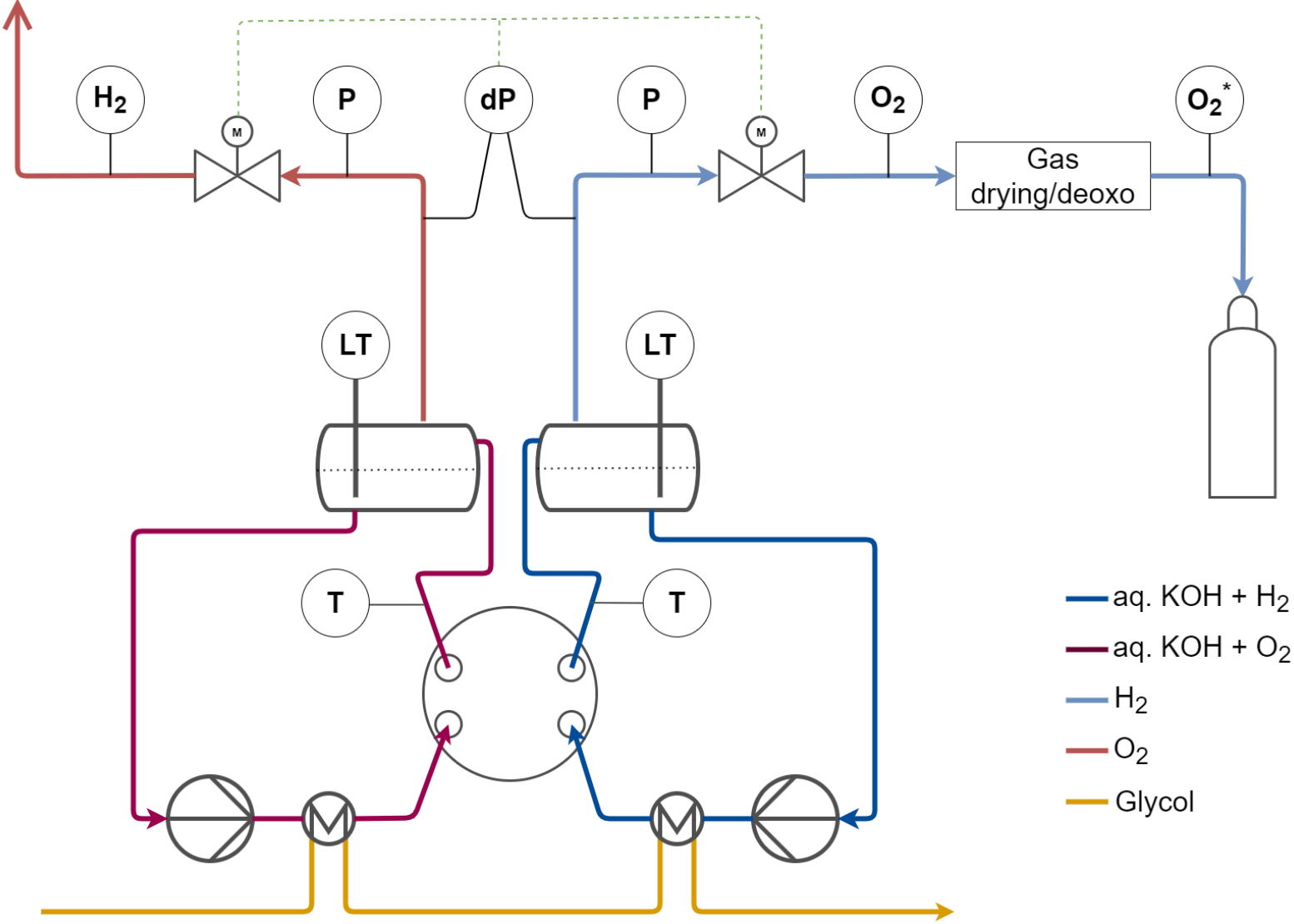
<53 kWh /kg H₂ (Stack energy requirement)



Instrumentation and operation

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MinWP Process diagram



Instrument requirements

Gas system

H₂ or O₂
compatible

AISI 316 or
similar

35-50
bar(g)

(P)AWE system

35% aq. KOH +
dissolved O₂/H₂

Ni or F

35-50 bar(g)

(P)PEM system

Water +
dissolved O₂/H₂

Pt, Ir (316L)

35+ bar(g)



Zone 2, Hydrogen,

Conclusion

The what (technology)



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Recap of technologies

Competitive dimension	Pressurised alkaline	PEM	Atmospheric alkaline
Flexibility Capacity to operate dynamically at variable load rates	✓	✓	✗
<i>Key for utilisation of renewable energy sources – across potential applications and minimisation of energy lost</i>			
Reliability System uptime and durability	✓	✓	✓
Efficiency Competitive energy to hydrogen conversion	✓	✓	✓
Footprint Minimal footprint compared to other electrolyser technologies	✓	✓	✗
Independency of scarce resources Noble metals not an input in process	✓	✗	✓
Water purity Lower water purity required in process	✓	✗	✓
Independency of lye The chemical lye is not contained in the electrolyser	✗	✓	✗



Technological viability has the potential to be a key competitive differentiator, as CAPEX costs between technologies are expected to converge in the long-run



Long term market differentiators could be centered around flexibility, reliability, efficiency (main OPEX driver) and footprint



Pressurised alkaline is well-positioned across competitive dimensions

Thank you



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HYDROGEN
SYSTEMS